

### AMENDMENTS TO THE CLAIMS

1. (Currently amended) A process for preparing methanol from a synthesis gas comprising carbon monoxide, carbon dioxide and hydrogen by steps of:

(a) passing the synthesis gas into a reactor containing a solid methanol conversion catalyst particles being suspended in a liquid phase of methanol and water;

(b) reacting the synthesis gas in presence of the suspended catalyst at a pressure and temperature, where methanol being formed on the catalyst condenses into the liquid phase; [[and]]

(c) withdrawing from the reactor a part of the liquid phase containing formed methanol product; and

(d) recycling a stream comprising methanol and at least one of the compounds of methyl formate and ethanol into the liquid phase obtained in step (b) to establish chemical equilibrium and to suppress formation of the at least one of the compounds.

2. (Currently amended) A process in accordance with claim 1, wherein the amount of water being present in the liquid phase is 0-10 wt%, ~~preferably 0-3 wt%.~~

3. (Currently amended) A process in accordance with claim 1, wherein the pressure in the slurry bed reactor is 50-290 bar, ~~preferentially 60-140 bar.~~

4. (Currently amended) A process in accordance with claim 1, wherein the temperature in the slurry bed reactor is between 150 °C to 240 °C, ~~preferentially 180-225 °C.~~

5. (Original) A process in accordance with claim 1, wherein the synthesis gas has a CO<sub>2</sub>/CO molar ratio of 0.02-1.0 and an H<sub>2</sub>/CO molar ratio of 2-4.

6. (Original) A process in accordance with claim 1, wherein the synthesis gas comprises 15-35 vol.% CO, 60-74 vol.% H<sub>2</sub> and 0-15 vol.% CO<sub>2</sub>.

7. (Original) A process of ~~claim~~ claim 1 further comprising of a step of recycling an effluent gas stream being withdrawn from the reactor.

8. (Original) A process of claim 1, wherein the reacting synthesis gas is cooled by internal cooling means.

9. (Original) A process of claim 1, wherein methanol and/or catalyst is added as fresh or being recycled to the reactor.

10. (Canceled)

11. (New) A process in accordance with claim 1, wherein the amount of water being present in the liquid phase is 0-3 wt%.

12. (New) A process in accordance with claim 1, wherein the pressure in the slurry bed reactor is 60-140 bar.

13. (New) A process in accordance with claim 1, wherein the temperature in the slurry bed reactor is 180-225 °C.